

# “Weakly Ligated, Labile Ligand” Nanoparticles: The Case of $\text{Ir}(0)_n \cdot (\text{H}^+ \text{Cl}^-)_m$

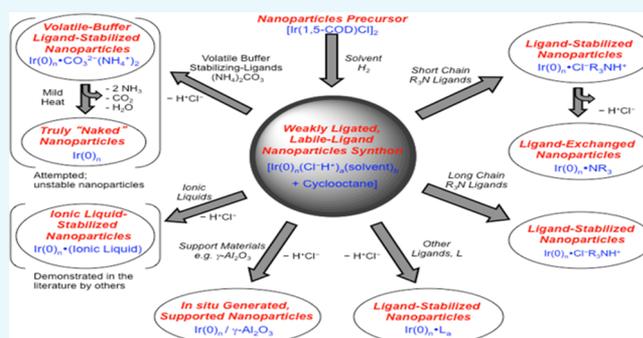
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## S Supporting Information

**ABSTRACT:** It is of considerable interest to prepare weakly ligated, labile ligand (WLLL) nanoparticles for applications in areas such as chemical catalysis. WLLL nanoparticles can be defined as nanoparticles with sufficient, albeit minimal, surface ligands of moderate binding strength to meta-stabilize nanoparticles, initial stabilizer ligands that can be readily replaced by other, desired, more strongly coordinating ligands and removed completely when desired. Herein, we describe WLLL nanoparticles prepared from  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  reduction under  $\text{H}_2$ , in acetone. The results suggest that  $\text{H}^+ \text{Cl}^-$ -stabilized  $\text{Ir}(0)_n$  nanoparticles, herein  $\text{Ir}(0)_n \cdot (\text{H}^+ \text{Cl}^-)_a$ , serve as a WLLL nanoparticle for the preparation of, as illustrative examples, five specific nanoparticle products:  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{Bu}_3\text{NH}^+)_a$ ,  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{Dodec}_3\text{NH}^+)_a$ ,  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n} (\text{Cl}^- \text{H}^+)_b$ ,  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n}$  and the  $\gamma\text{-Al}_2\text{O}_3$ -supported heterogeneous catalyst,  $\text{Ir}(0)_n \cdot (\gamma\text{-Al}_2\text{O}_3)_a (\text{Cl}^- \text{H}^+)_b$ . (where  $a$  and  $b$  vary for the differently ligated nanoparticles; in addition, solvent can be present as a nanoparticle surface ligand). With added  $\text{POct}_3$  as a key, prototype example, an important feature is that a minimum, desired, experimentally determinable amount of ligand (e.g., just 0.2 equiv  $\text{POct}_3$  per mole of Ir) can be added, which is shown to provide sufficient stabilization that the resultant  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n} (\text{Cl}^- \text{H}^+)_b$  is isolable. Additionally, the initial labile ligand stabilizer  $\text{HCl}$  can be removed to yield  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n}$  that is >99% free of  $\text{Cl}^-$  by a  $\text{AgCl}$  precipitation test. The results provide strong support for the weakly ligated, labile ligand nanoparticle concept and specific support for  $\text{Ir}(0)_n \cdot (\text{H}^+ \text{Cl}^-)_a$  as a WLLL nanoparticle.



## INTRODUCTION

Transition-metal nanoparticles are of significant interest within the catalysis community.<sup>1–5</sup> Because bulk metal is thermodynamically favored compared to metal(0) nanoparticles, stabilizing ligands are needed to prevent agglomeration of the resultant nanoparticles in solution.<sup>6</sup> Unfortunately, many (albeit not all<sup>7</sup>) common stabilizers bind strong enough to nanoparticle catalyst surfaces to act as catalyst poisons.<sup>8,9</sup> This includes many of the ligands that have led to what are otherwise valuable advances in the synthesis of size- and shape-controlled transition-metal nanoparticles.<sup>10–15</sup>

There have been many attempts to remove nanoparticle surface ligands, including extensive treatments such as thermal activation in  $\text{N}_2$ ,  $\text{H}_2$ , and  $\text{O}_2$  environments,<sup>16–20</sup> UV/ozone,<sup>21–25</sup>  $\text{O}_2$ /plasma,<sup>24</sup> and neutron sputtering.<sup>26</sup> Complete (100%) removal of nanoparticle-stabilizing ligands and polymers without inducing nanoparticle agglomeration or oxidizing the nanoparticle surface has proven largely unsuccessful, not unexpectedly.<sup>17–21,23,24</sup> A related problem of current interest is establishing and controlling a precise nanoparticle surface composition,<sup>27</sup> ill-defined and uncontrolled nanoparticle composition in turn affecting key catalytic

properties such as catalytic selectivity, activity, lifetime, recovery, and recyclability.<sup>28</sup>

There have also been a number of reports attempting to prepare putatively “naked” nanoparticles that, in at least the literal interpretation of naked, would be devoid of any ligands, even solvent.<sup>8,29–34</sup> Although there have been claims of naked nanoparticles in the literature,<sup>35–37</sup> nanoparticle surfaces will of course never be truly naked in solution because even solvent-to-metal bond energies are  $10 \pm 3$  kcal/mol for even the extreme case of metal–alkane bonds, at least in small-molecule organometallic complexes.<sup>38–41</sup> Solvent-only stabilized nanoparticles have been claimed in the literature,<sup>42–46</sup> but often anionic ligands (such as  $\text{Cl}^-$ ,  $\text{OAc}^-$ , or other anions present in the synthetic precursor) are present but have not been tested, nor hence ruled out, as actual sources of nanoparticle stabilization. For example, in a recent report,<sup>35</sup>  $\text{Pt}(0)$  nanoparticles generated in acetic acid are claimed to be naked, but the high probability of surface  $\text{OAc}^-$  as a stabilizing ligand was not tested nor ruled out. We discuss putatively

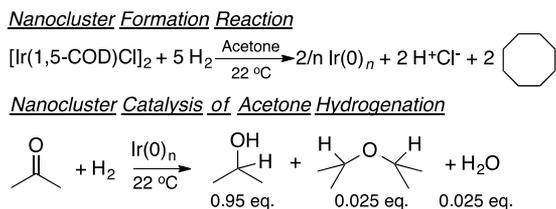
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naked nanoparticles more in the Supporting Information (SI) for the interested reader.

**Scheme 1. Nanoparticle Formation Stoichiometry and Acetone Hydrogenation Activity of  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{H}^+)_a (\text{acetone})_b$  WLLL Nanoparticles Starting from  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  in Neat Acetone at 22 °C under an Initial 3.7 atm of  $\text{H}_2$** <sup>59</sup>



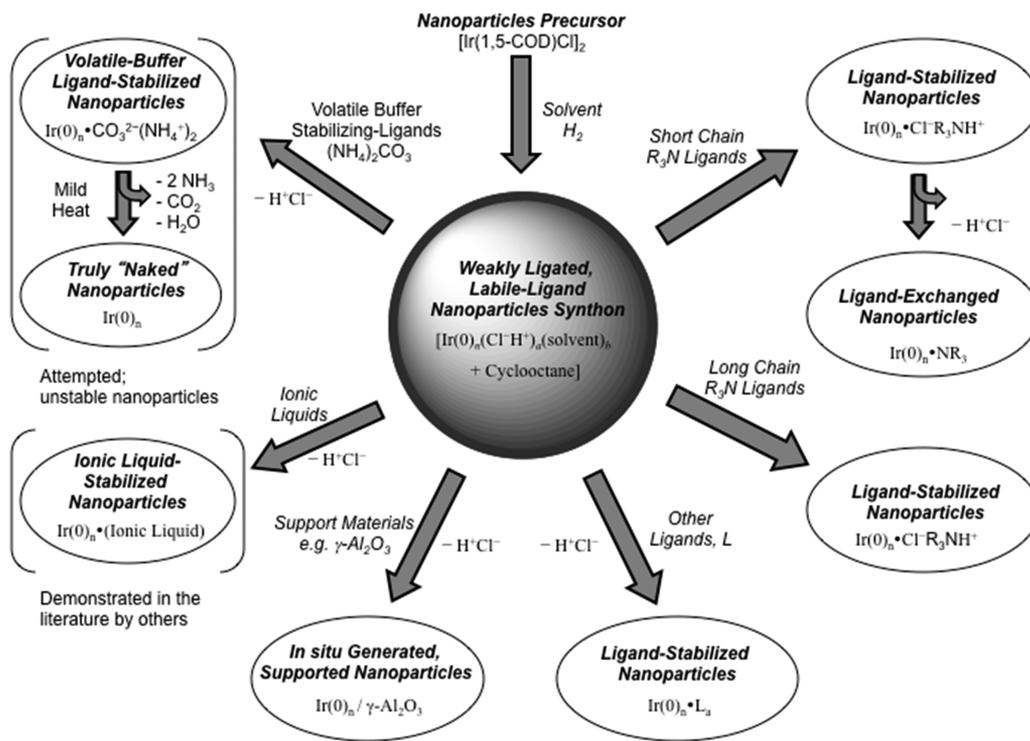
Hence, an unrealized goal is to prepare nanoparticles that have only relatively weakly bound, kinetically labile ligands, which provide a near-minimum level of nanoparticle meta-stabilization, which we have termed “weakly ligated, labile ligand” (WLLL) nanoparticles.<sup>6,38,47</sup> Such nanoparticles could, then and in principle, serve as a key synthetic structural unit/building block—that is, as a (nanoparticle) synthon—for use in the preparation of differently ligated nanoparticles and other nanoparticle products, the word synthon having been coined by Corey in 1967.<sup>48</sup> Such nanoparticles would then have a relatively precise, well-defined set of (at least average) ligands, plus any bound solvent, for applications in catalysts and other areas. It would be valuable synthetically to be able to add

pretty much any desired ligand to a nanoparticle synthon, especially if sub-stoichiometric amounts (ligand/metal  $\ll 1$ ) could be used thereby leaving surface sites available—that is, providing coordinative unsaturation—for catalysis or other applications and also opening up the use of the ligand/metal ratio for nanoparticle size and catalytic activity control.<sup>49–52</sup>

Worth noting here is that minimally stabilized, meta-stable, substitutionally labile metal complexes that are (or behave as if they are) coordinatively unsaturated are an important concept in classical organometallic chemistry. Notable here are complexes such as Wilke’s classic “naked nickel”,  $\text{Ni}^0(1,5\text{-COD})_2$ ,<sup>53</sup>  $\text{M}(1,5\text{-COD})_2^{n+}$  or  $\text{M}(1,5\text{-COD})\text{Cl}_x$  ( $\text{M} = \text{Ir}, \text{Rh}, \text{Pt}, \text{Ru}$ ),<sup>54,55</sup>  $\text{M}(\text{NCCH}_3)_x^{n+}(\text{BF}_4)_n$  complexes ( $\text{M} = \text{Mn}^{\text{II}}, \text{Fe}^{\text{II}}, \text{Co}^{\text{II}}, \text{Cu}^{\text{II}}, \text{Cu}^{\text{I}}, \text{Zn}^{\text{II}}$ ),<sup>56</sup> as well as other examples one can find in the literature.<sup>57,58</sup> Indeed,  $\text{Ir}(1,5\text{-COD})\text{Cl}_2$  is a key starting material in the present contribution. It follows that development of lightly stabilized, meta-stable, effectively coordinatively unsaturated, WLLL nanoparticles can be expected to have an analogous, sizable, positive impact on nanoparticle science.

We previously reported that  $\text{Ir}(0)$  nanoparticles obtained from  $\text{H}_2$  reduction of  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  in acetone are formed according to the balanced reaction in Scheme 1.<sup>59</sup> By design, this simple, clean reaction produces  $\text{Ir}(0)$  nanoparticles<sup>59,60</sup> that have only two possibilities for surface ligands,  $\text{H}^+\text{Cl}^-$  and acetone solvent, that is,  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{H}^+)_a (\text{acetone})_b$ —and as such, they are a prototype example of WLLL nanoparticles. The formation of discrete  $1.8 \pm 0.5$  nm  $\text{Ir}(0)_n$  nanoparticles is evident from transmission electron microscopy (TEM) imaging of a sample harvested at an early stage of the acetone

**Scheme 2. Formation and Possible Applications of  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{H}^+)_a (\text{acetone})_b$  as a Weakly Ligated, Labile Ligand (WLLL) Precursor**<sup>61</sup>



<sup>61</sup>The  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{H}^+)_a (\text{acetone})_b$  is shown as a true synthon in the scheme to illustrate the concept; it should be noted, however, that, in the present work, the  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{H}^+)_a (\text{acetone})_b$  is not pre-made or preisolated, but rather is formed in situ with the added ligands such as  $\text{R}_3\text{N}$  and  $\text{POCl}_3$ , or solid support,  $\gamma\text{-Al}_2\text{O}_3$ .

hydrogenation reaction, as shown in Figure 1 of the original paper.<sup>59</sup>

Pleasingly, the  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{H}^+)_a (\text{acetone})_b$  nanoparticles proved to be an exceptionally active and selective acetone hydrogenation catalyst (1.9 turnovers/s at 22 °C to 95% 2-propanol; 16 400 total catalytic turnovers).<sup>59</sup> The acid-assisted catalytic hydrogenation of acetone was corroborated by the inhibition of catalysis (no catalytic turnover) if  $\text{H}^+$  is scavenged from solution by using Proton Sponge (1,8-bis-(dimethylamino)naphthalene) as a strong, noncoordinating base<sup>62</sup> and by the unusual kinetics of the reaction that were, however, explicable in terms of the HCl requirement for acetone hydrogenation.<sup>59</sup>

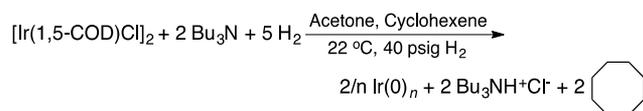
The above results, while encouraging and quite supportive of the WLLL nanoparticle concept, left a number of additional, remaining possible uses of the WLLL  $\text{Ir}(0)_n$  nanoparticles to be examined (Scheme 2). We note that others have already contributed to this scheme, notably the ionic liquid studies from Dupont's labs that will be referenced and detailed in a later section.

Herein, we report the additional studies probing the WLLL nanoparticle concept in the case of  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{H}^+)_a (\text{acetone})_b$  of: (i) adding  $\text{Bu}_3\text{N}$  to make  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{Bu}_3\text{NH}^+)_b$  nanoparticles; (ii) subsequently removing  $\text{H}^+ \text{Cl}^-$  to yield  $\text{Ir}(0)_n \cdot (\text{NBu}_3)_c$  nanoparticles; (iii) adding longer-chain Dodec<sub>3</sub>N to yield  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{Dodec}_3\text{NH}^+)_b$  nanoparticles; and importantly (iv) adding  $\text{POct}_3$  and removing  $\text{H}^+ \text{Cl}^-$  to yield  $\text{Ir}(0)_n \cdot (\text{POct}_3)_d$  catalytically active nanoparticles, where the ratio of  $\text{POct}_3/\text{Ir}$  is small, 0.1–0.2. In addition, we report (v) adding  $\gamma\text{-Al}_2\text{O}_3$  (and removing  $\text{H}^+ \text{Cl}^-$ ) to yield  $\text{Ir}(0)_n \cdot \gamma\text{-Al}_2\text{O}_3$  catalytically active nanoparticles. The results suggest that  $\text{Ir}(0)_n \cdot \text{H}^+ \text{Cl}^-$  can serve as a WLLL en route to composition- and surface ligand-controlled nanoparticles for catalysis and other applications.

## RESULTS AND DISCUSSION

**$\text{Bu}_3\text{NH}^+ \text{Cl}^-$ -Stabilized Nanoparticles from  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  Plus  $\text{Bu}_3\text{N}$ .** Starting with  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$ ,  $\text{Bu}_3\text{NH}^+ \text{Cl}^-$ -stabilized  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{Bu}_3\text{NH}^+)_a$  nanoparticles were synthesized in acetone under  $\text{H}_2$  and now in the presence of 1 equiv  $\text{Bu}_3\text{N}$  (Scheme 3).

### Scheme 3. Stoichiometry of Formation of $\text{Bu}_3\text{NH}^+ \text{Cl}^-$ -Stabilized $\text{Ir}(0)_n$ Nanoparticles



The stoichiometry of the reaction was confirmed via cyclooctane evolution, where  $1.0 \pm 0.1$  equiv per mole of Ir were evolved. The reaction was monitored indirectly by having 1375 equiv of cyclohexene (vs Ir) present, that is, by our well-precedented method of a cyclohexene hydrogenation reporter reaction that reports the formation of catalytically active  $\text{Ir}(0)_n$  nanoparticles (Figure 1).<sup>59</sup> Note that the evolution of  $1.0 \pm 0.1$  equiv cyclooctane per Ir and no detectible amount of cyclohexene after hydrogenation (as determined by gas chromatography (GC) and NMR) indicate the complete conversion of cyclohexene to cyclohexane. Hence, no cyclohexene remains so that cyclohexene needs not be considered as a possible nanoparticle surface ligand. The resultant  $\text{Ir}(0)_n \cdot$

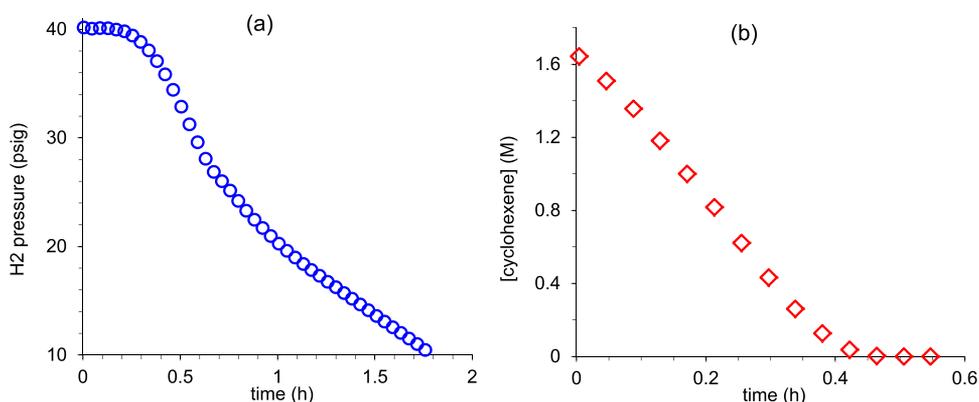
$\text{Bu}_3\text{NH}^+ \text{Cl}^-$  nanoparticles shown in Figure 2 have an average size of  $1.8 \pm 0.6$  nm.

A control reaction, to test if the hydrogenation is influenced by mass-transfer limitations<sup>63</sup> even though the reaction is well stirred, was done in which the same  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  and  $\text{Bu}_3\text{N}$  precursors were used, but each was concentration-doubled. The results, given in Figure S1 of the Supporting Information, show that the cyclohexene hydrogenation rate is doubled in comparison to that given in Figure 1b, demonstrating that the reaction is not under  $\text{H}_2$  gas-to-solution mass-transfer limitations.<sup>63</sup>

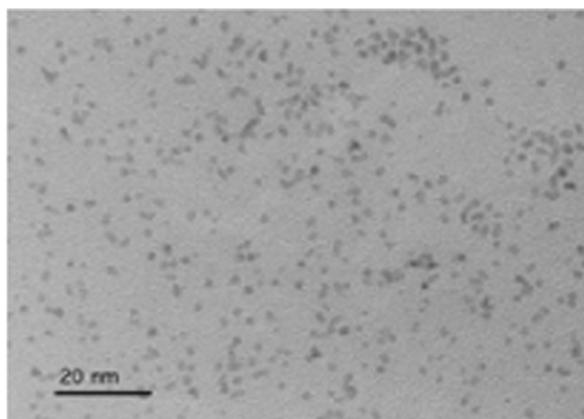
The  $\text{Bu}_3\text{NH}^+ \text{Cl}^-$ -stabilized  $\text{Ir}(0)_n$  nanoparticles are active cyclohexene hydrogenation catalysts, providing an initial TOF of  $1.1 \text{ s}^{-1}$  at  $22.0 \pm 0.1$  °C (Figure 1b). The nanoparticles can also be redispersed in acetone solution, retaining a TOF value of  $0.2 \text{ s}^{-1}$  at  $22.0 \pm 0.1$  °C (Figure S2 in the SI) and yielding 25 000 total turnovers (TTOs) for cyclohexene reduction before deactivating via agglomeration (Figure S3 in the SI and in comparison to Figure S2). In short, compositionally relatively simple and relatively well-defined, catalytically active  $\text{Bu}_3\text{NH}^+ \text{Cl}^-$ -stabilized  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{Bu}_3\text{NH}^+)_a$  nanoparticles have been prepared from the in situ generated  $\text{Ir}(0)_n \cdot \text{H}^+ \text{Cl}^-$  in the presence of  $\text{Bu}_3\text{N}$ , as shown back in Scheme 2.

**Demonstration of  $\text{H}^+ \text{Cl}^-$  Removal from  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{Bu}_3\text{NH}^+)_a$ .** To demonstrate the extent to which the weak, initially present labile ligand  $\text{H}^+ \text{Cl}^-$  could be removed from the  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{Bu}_3\text{NH}^+)_a$  nanoparticles, the solid particles were heated from 100 to 300 °C under He in a thermogravimetric analysis (TGA) experiment. The thermogravimetric analysis (TGA) data in Figure 3 show a weight loss of 8.6% between 25 and 120 °C, indicating that  $\geq 98\%$  of the HCl can be removed under the relatively mild TGA,  $\leq 120$  °C conditions. (It is likely that the other,  $\leq 2\%$  of HCl, was removed when the solvent and cyclohexane (resulting from the hydrogenation of cyclohexene) were removed under vacuum from the sample at room temperature, prior to the TGA analysis.) The 16.6% weight loss between 120 and 200 °C is attributed to partial removal of the resultant  $\text{Bu}_3\text{N}$  ligand (theoretical for the full loss of  $\text{Bu}_3\text{N} = 44.8\%$ ). Interestingly, the resultant  $\text{Bu}_3\text{N}$ -stabilized nanoparticles are partially, albeit not completely, stabilized against agglomeration when resuspended in acetone solution (see Figure S2 in the SI for details).

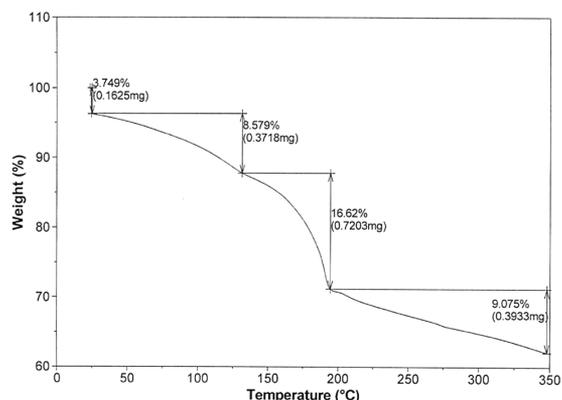
Of note here is that these results are interesting when considered in light of classic heterogeneous catalysis literature, where removal of  $\text{Cl}^-$  from the active metal surface is important because  $\text{Cl}^-$  is well known to affect catalytic rates, for example benzene hydrogenation over  $\text{Ir}/\text{TiO}_2$  catalysts.<sup>64</sup> Additionally,  $\text{Cl}^-$  removal is crucial when trying to deconvolute trace  $\text{Cl}^-$  effects from the effects of changing facet ratios that accompany decreasing nanoparticle size.<sup>65</sup> In general, and despite extensive efforts to remove  $\text{Cl}^-$  quantitatively from supported catalysts, complete  $\text{Cl}^-$  removal from  $\text{MCl}_x \cdot (\text{H}_2\text{O})_n$  plus  $\text{H}_2$  (and which in principle generates  $\text{M}(0) \cdot \text{HCl}$ , not unlike the present syntheses) is a difficult task,<sup>64,66,67</sup> with, for example, demonstration of observable catalytic activity suppression at a  $\text{Cl}^-/\text{Au}$  molar ratio as low as 0.0006.<sup>67</sup> A compounding problem is that the waters of solvation can change the putative " $\text{MCl}_x \cdot (\text{H}_2\text{O})_n$ " to a more complex speciation that involves  $\text{MCl}_{x-2y} \text{O}_y (\text{H}_2\text{O})_{n-y} \cdot 2y(\text{HCl})$ , not all of which are as readily or cleanly reducible to  $\text{M}(0)$  as is, for example, the  $[(1,5\text{-COD})\text{IrCl}]_2$  precatalyst employed herein. However, by starting herein with the well-defined, already



**Figure 1.** (a) Hydrogen uptake vs time plot for the hydrogenation of cyclohexene plus acetone and concomitant formation of iridium(0) nanoparticles starting with  $[(1,5\text{-COD})\text{IrCl}]_2$  (1.2 mM Ir) and cyclohexene (1.65 M) in acetone at  $22.0 \pm 0.1$  °C. Both cyclohexene and acetone undergo hydrogenation; the former is faster than the latter.<sup>59</sup> (b) Loss of cyclohexene versus time curve in the hydrogenation of 1.65 M cyclohexene and concomitant formation of Ir(0) nanoparticles starting with  $[(1,5\text{-COD})\text{IrCl}]_2$  (1.2 mM Ir) and 1.2 mM  $\text{Bu}_3\text{N}$  in acetone at  $22.0 \pm 0.1$  °C. A linear hydrogenation of cyclohexene starts with an initial turnover frequency (TOF) of  $1.1 \text{ s}^{-1}$ . The pressure rise in the initial part of both curves (not shown), due to the solvent vapor pressure reequilibration after 15 flushes of the reaction flask with  $\text{H}_2$ , has been corrected (and thereby removed from this curve as) by the preceded procedure described elsewhere.<sup>61</sup>



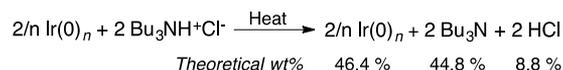
**Figure 2.** TEM image of  $\text{Ir}(0)_n$  nanoparticles sample harvested after complete cyclohexene hydrogenation starting with  $[(1,5\text{-COD})\text{IrCl}]_2$  (1.2 mM Ir) and 1.2 mM  $\text{Bu}_3\text{N}$  in acetone at  $22.0 \pm 0.1$  °C. The average particle size is  $1.8 \pm 0.6$  nm.



**Figure 3.** TGA of the  $\text{Bu}_3\text{NH}^+\text{Cl}^-$ -stabilized  $\text{Ir}(0)_n$  nanoparticles formed during the reduction of 3.6 mM  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  in the presence of 7.2 mM  $\text{Bu}_3\text{N}$  in acetone at 22 °C and under an initial pressure of 4.7 atm  $\text{H}_2$  along with concomitant hydrogenation of an initial 1.65 M cyclohexene. The observed 8.6 wt % loss from 25 to 120 °C is attributable to the removal of  $\geq 98\%$  of the  $\text{HCl}$  present (i.e., 8.6% weight loss vs a theoretical 8.8% loss).

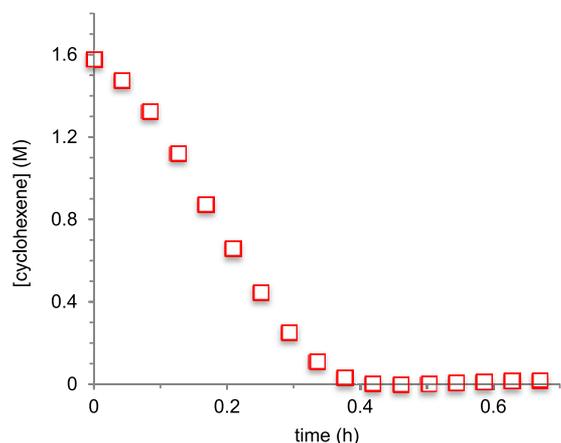
partially reduced (to Ir(I)) precursor  $[(1,5\text{-COD})\text{IrCl}]_2$  (which, for example, lacks undesired waters of solvation), the reduction under  $\text{H}_2$  proceeds cleanly and quantitatively to  $\text{Ir}(0)\cdot\text{H}^+\text{Cl}^-$  according to the stoichiometry shown back in Scheme 1. The resultant, volatile  $\text{HCl}$  is then readily removable under relatively mild,  $\leq 120$  °C conditions (Scheme 4).

**Scheme 4. Stoichiometry and Theoretical Weight Loss Percentages for the Removal of Volatile  $\text{H}^+\text{Cl}^-$  from  $\text{Ir}(0)_n\cdot\text{Cl}^-\text{Bu}_3\text{NH}^+$  by Mild,  $\leq 120$  °C Heating**

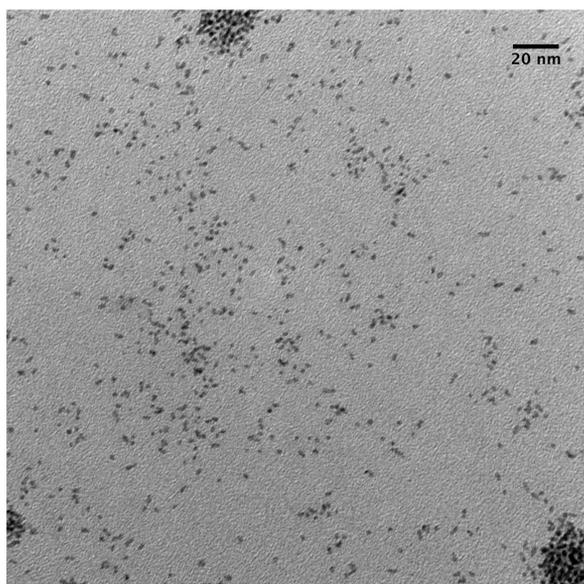


**Extension to Longer-Chain Amine-Stabilized Nanoparticles: Dodec<sub>3</sub>NH<sup>+</sup>Cl<sup>-</sup>-Stabilized Nanoparticles  $\text{Ir}(0)_n\cdot(\text{Cl}^-\text{Dodec}_3\text{NH}^+)_a$  from  $\text{H}_2$  Reduction of  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  in the Presence of Dodec<sub>3</sub>N.** To demonstrate the ready extension of the WLL nanoparticle route to longer-chain amines that can, therefore, serve as enhanced stabilizers or render different nanoparticle solubility,<sup>6</sup>  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  was reduced under  $\text{H}_2$  in acetone solution at  $22.0 \pm 0.1$  °C in the presence of tris(dodecyl)amine as an additional nanoparticle stabilizer as well as in the presence of 1.65 M cyclohexene (that, again, is completely hydrogenated as demonstrated by GC and NMR and, therefore, not available as an olefinic ligand stabilizer; Figure 4).

Dodec<sub>3</sub>NH<sup>+</sup>Cl<sup>-</sup>-stabilized  $\text{Ir}(0)_n$  nanoparticles show cyclohexene hydrogenation activity (initial TOF of  $\sim 1.4 \text{ s}^{-1}$ ) essentially the same as that of  $\text{Bu}_3\text{NH}^+\text{Cl}^-$ -stabilized  $\text{Ir}(0)_n$  nanoparticles (initial TOF of  $1.1 \text{ s}^{-1}$ ) at  $22.0 \pm 0.1$  °C (Figure 4). The nanoparticles can be redispersed in acetone solution, retaining a TOF value of  $0.2 \text{ s}^{-1}$  in the second run of cyclohexene hydrogenation at  $22.0 \pm 0.1$  °C (Figure S4 in the SI). The TEM image (Figure 5) shows that the Dodec<sub>3</sub>NH<sup>+</sup>Cl<sup>-</sup>-stabilized  $\text{Ir}(0)_n$  nanoparticles have an average particle size of  $1.8 \pm 0.6$  nm, the same within experimental error as the  $\text{Bu}_3\text{NH}^+\text{Cl}^-$ -stabilized  $\text{Ir}(0)_n$  nanoparticles. These results demonstrate that changing the alkyl chain length by eight carbons from butyl to dodecyl has no significant



**Figure 4.** Loss of cyclohexene vs time curve in the  $H_2$  reduction of  $[(1,5\text{-COD})\text{IrCl}]_2$  (1.2 mM Ir) in the presence of 1.2 mM Dodec<sub>3</sub>N in acetone at  $22.0 \pm 0.1$  °C along with concomitant complete hydrogenation of 1.65 M cyclohexene. The pressure rise observed in the initial part of the curve, due to the solvent vapor pressure reequilibration after 15 flushes of the reaction flask with  $H_2$ , has been corrected (and hence removed from this curve) by the preceded procedure described elsewhere.<sup>61</sup>



**Figure 5.** TEM image of  $\text{Ir}(0)_n$  nanoparticles harvested after complete cyclohexene hydrogenation starting with  $[(1,5\text{-COD})\text{IrCl}]_2$  (1.2 mM Ir) and 1.2 mM tris(dodecyl)amine, Dodec<sub>3</sub>N in acetone at  $22.0 \pm 0.1$  °C. The average particle size is  $1.8 \pm 0.6$  nm.

influence on the particle size or catalytic activity of the resultant  $R_3\text{NH}^+\text{Cl}^-$ -stabilized  $\text{Ir}(0)_n$  nanoparticles.

**$\text{POct}_3$ -Stabilized  $\text{Ir}(0)_n$  Nanoparticles,  $\text{Ir}(0)_n \cdot (\text{POct}_3)_a(\text{Cl}^- \text{H}^+)_b$ , from  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  Plus  $\text{POct}_3$ .** Starting with  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  plus just 0.2 equiv  $\text{POct}_3$  per mole of iridium in acetone,  $\text{Ir}(0)_n \cdot (\text{POct}_3)_a(\text{Cl}^- \text{H}^+)_b$  nanoparticles were formed during the cyclohexene/acetone hydrogenation under  $H_2$  at  $22.0 \pm 0.1$  °C (Figure 6a). Trioctylphosphine was picked based on a suggestion from our collaborator Prof. A. Karim and because it is a strongly binding ligand with a perhaps surprisingly small Tolman cone angle of  $107^\circ$  (in comparison to  $\text{PR}_3$  ( $R = \text{Et}, \text{Pr}, \text{Bu}$ ) cone angles that are all  $132^\circ$ ).<sup>68</sup> Importantly, adding just 0.2 equiv  $\text{POct}_3$  per mole of Ir to the starting  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  precatalyst solution yields

stable iridium(0) nanoparticles that are still active hydrogenation catalysts. In short, the  $\text{Ir}(0)_n \cdot (\text{Cl}^- \text{H}^+)_b$  WLLL concept leads to the ready preparation of  $\text{Ir}(0)_n \cdot (\text{POct}_3)_a(\text{Cl}^- \text{H}^+)_b$  nanoparticles with an approximately (low level) minimum amount of added ligand,  $L = (\text{POct}_3)$  in this case, which yields a narrow,  $1.5 \pm 0.2$  nm dispersion of catalytically active  $\text{Ir}(0)_n$  nanoparticles with no visibly or TEM-discernable bulk metal.

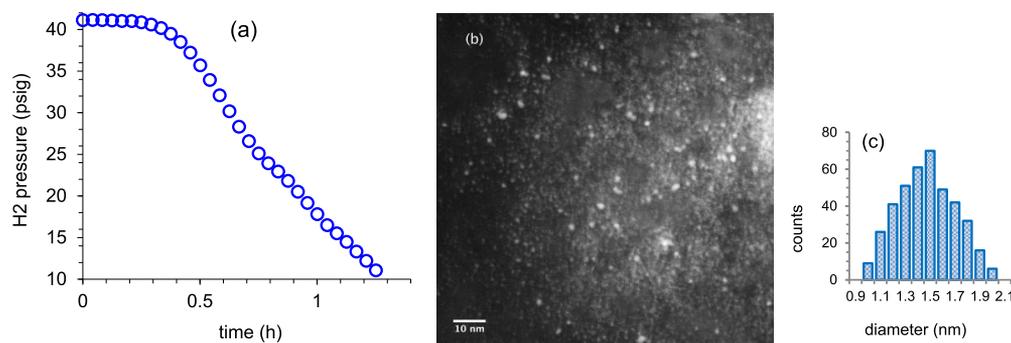
Figure 6b shows TEM image of the sample harvested after the complete hydrogenation of cyclohexene and acetone (22 h) exhibiting the formation of highly dispersed  $\text{Ir}(0)_n$  nanoparticles. The GC determination of  $1.0 \pm 0.1$  equiv of cyclooctane evolution per mole of Ir after 22 h indicates the complete reduction of the (1,5-COD)Ir(I)-containing precursor to  $\text{Ir}(0)$  when the nanoparticle sample harvested. The average particle size is  $1.5 \pm 0.2$  nm according to the histogram in Figure 6c. The comparison of the particle size of  $\text{Ir}(0)_n \cdot (\text{POct}_3)_a(\text{Cl}^- \text{H}^+)_b$  to that of  $\text{Bu}_3\text{NH}^+\text{Cl}^-$  or  $\text{Dodec}_3\text{NH}^+\text{Cl}^-$ -stabilized nanoparticles ( $1.8 \pm 0.6$  nm) is consistent with the effect of the stronger binding  $\text{POct}_3$  phosphine ligand yielding an on average smaller,  $\geq 3$  fold-narrower size distribution of  $\text{Ir}(0)_n \cdot (\text{POct}_3)_a(\text{Cl}^- \text{H}^+)_b$  nanoparticles.

Noteworthy here is that ligand-based control of nanoparticle sizes and size distributions is an important current research topic.<sup>9,45,69–71</sup> The  $\text{Ir}(0)_n \cdot (\text{POct}_3)_a(\text{Cl}^- \text{H}^+)_b$  system developed herein is important in this regard because well-formed and size-controlled  $\text{Ir}(0)_{\sim 150}$  nanoparticles<sup>4,72,73</sup> are formed from even low, 0.2 equiv ligand-to-Ir ratios—implying, in turn, that ligand-to-Ir ratios between 0.2 and  $\geq 1.0$  should be studiable by in-progress small-angle X-ray scattering (SAXS) and other efforts.

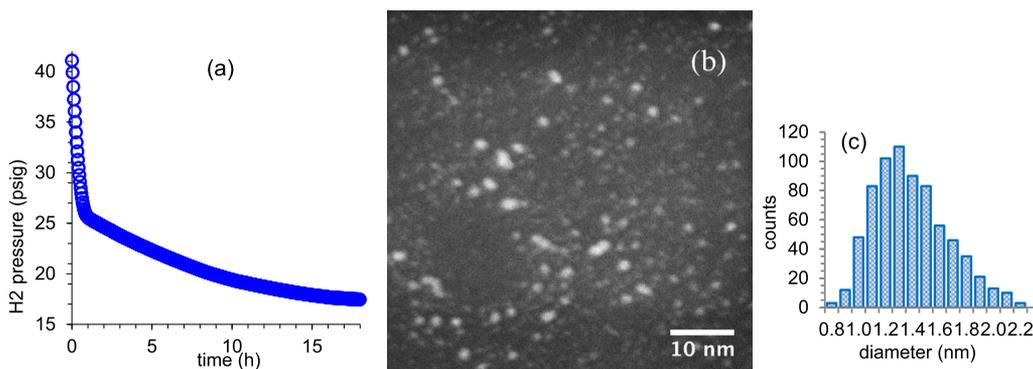
**Isolable, HCl-free, Minimally Ligated  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n}$  Nanoparticles.** Significantly, trioctylphosphine-stabilized  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n}$  nanoparticles, with only 0.2 equiv of  $\text{P}(\text{Oct})_3$  and testing  $\geq 99\%$  free of HCl, could be isolated as a powder by removing HCl and the acetone solvent under vacuum. It is noteworthy that these isolated  $\text{Ir}(0)$  nanoparticles are redispersible in acetone and other organic solvents with good catalytic activity: Figure 7a shows the  $H_2$  uptake versus time plot cyclohexene plus acetone hydrogenation using the isolated  $\text{Ir}(0)_n$  nanoparticles formed from a first run of cyclohexene/acetone hydrogenation. Compared to the  $\text{Ir}(0)_n \cdot (\text{POct}_3)_a(\text{Cl}^- \text{H}^+)_b$  nanoparticles (Figure 6c, where the mean particle size is  $1.5 \pm 0.2$  nm, i.e.,  $\pm 15\%$ ), the  $\text{Ir}(0)_n \cdot (\text{POct}_3)_a$  nanoparticles do exhibit a somewhat broadened size distribution (Figure 7c, the mean particle size =  $1.4 \pm 0.4$  nm, i.e.,  $\pm 28\%$ ), not unexpectedly because of some agglomeration during the isolation and redispersion processes.

However and significantly, HCl has been largely removed as demonstrated by the very slow hydrogenation of acetone seen in Figure 7 ( $\sim 0.91$  psig  $H_2$  loss/h), HCl being a known requirement for facile acetone hydrogenation (i.e., by the same precatalyst and under essentially identical conditions<sup>59</sup>).

Independently, confirming evidence for the removal of HCl at the  $>99\%$  level (i.e., from HCl-containing,  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n}(\text{Cl}^- \text{H}^+)_b$  nanoparticles) to give the novel, essentially HCl-free  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n}$  nanoparticles is provided by treatment of the isolated product with a 1.2 mM  $\text{AgBF}_4$  solution in acetone (the same concentration as the initial  $[(1,5\text{-COD})\text{IrCl}]_2$  precursor concentration). No visually observable precipitation of  $\text{AgCl}$  is seen, confirming the expected removal of HCl during the evacuation step to yield the HCl-free  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2n}$  product. To establish the limit



**Figure 6.** (a) Hydrogen uptake vs time plot for the hydrogenation of cyclohexene/acetone and concomitant formation of  $\text{Ir}(0)_n$  nanoparticles starting with  $[(1,5\text{-COD})\text{IrCl}]_2$  (1.2 mM Ir) plus 0.2 equiv  $\text{POct}_3$  and cyclohexene (1.65 M) in acetone at  $22.0 \pm 0.1$  °C. The pressure rise observed in the initial part of curve, due to the solvent vapor pressure reequilibration after 15 flushes of the reaction flask with  $\text{H}_2$ , has been corrected (and hence removed from this curve) by the precedent procedure described elsewhere.<sup>61</sup> (b) Bright-field scanning transmission electron microscopy (STEM) image and (c) the corresponding particle size histogram of  $\text{Ir}(0)_n(\text{POct}_3)_a(\text{Cl}^- \text{H}^+)_b$  nanoparticles in the sample harvested after 22 h hydrogenation (1.0  $\pm$  0.1 equiv cyclooctane had evolved as determined by GC). The mean diameter of  $\text{Ir}(0)$  nanoparticles is  $1.5 \pm 0.2$  nm (i.e.,  $\pm 15\%$ ).



**Figure 7.** (a) Hydrogen consumption vs time plot for the hydrogenation of cyclohexene (the fast part of the  $\text{H}_2$  pressure loss curve) then acetone (the slower, subsequent part of the hydrogenation curve) using the redispersed  $\text{Ir}(0)_n(\text{POct})_{0.2n}$  nanoparticles formed from a first run of cyclohexene/acetone hydrogenation (i.e., formed starting with  $[(1,5\text{-COD})\text{IrCl}]_2$  (1.2 mM Ir) plus 0.2 equiv  $\text{POct}_3$  and cyclohexene (1.65 M) in acetone at  $22.0 \pm 0.1$  °C). The  $\text{Ir}(0)$  nanoparticles were isolated by removing the volatiles including  $\text{HCl}$  in vacuum and then redispersed in acetone for this second hydrogenation. The pressure rise observed in the initial part of the curve, due to the solvent vapor pressure reequilibration after 15 flushes of the reaction flask with  $\text{H}_2$ , has been corrected (and hence removed from this curve) by the precedent procedure described elsewhere.<sup>61</sup> (b) Bright-field STEM image of the sample harvested after 22 h hydrogenation and (c) the corresponding particle size histogram of  $\text{Ir}(0)_n(\text{POct}_3)_{0.2n}$  nanoparticles. Mean diameter of  $\text{Ir}(0)$  nanoparticles is  $1.4 \pm 0.4$  nm (i.e.,  $\pm 28\%$ ).

of  $\text{Cl}^-$  (and thus  $\text{HCl}$ ) detectability in the added  $\text{Ag}^+$  experiment, a control was performed with 0.012 mM  $\text{Bu}_4\text{N}^+\text{Cl}^-$  (i.e., 1% relative to 1.2 mM Ir) plus 1.2 mM  $\text{AgBF}_4$  in acetone: a readily visualized  $\text{AgCl}$  precipitate is seen, in turn showing that even a 1% level of residual  $\text{Cl}^-$  would have been easily detected by the above simple, effective,  $\text{AgCl}$  precipitation test. Taken together, the results demonstrate that the  $\text{HCl}$  has been removed at the  $>99\%$  level from the  $\text{Ir}(0)_n(\text{POct}_3)_{0.2n}(\text{Cl}^- \text{H}^+)_b$  nanoparticle sample. The resultant desired, isolable, and redispersible, yet still highly catalytically active  $\text{Ir}(0)_n(\text{POct}_3)_{0.2n}$  nanoparticles possess a by-design low level of ligation that, however, is sufficient to allow the nanoparticles to be both isolated and then redispersed.

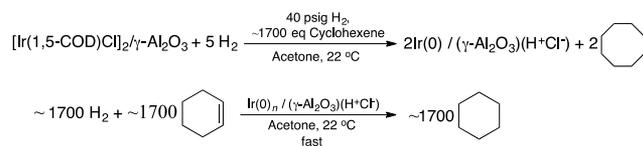
Note that a roughly average  $\text{Ir}(0)_{\sim 150}$  nanoparticle has ca. 0.6 of its total Ir atoms on the surface of the nanoparticle so that one expects the 0.2 equiv of  $\text{POct}_3$  present to be tightly bound in the as-formulated,  $\text{Ir}(0)_n(\text{POct}_3)_{0.2n}$  nanoparticles. While clearly much more remains to be done further characterizing and studying the  $\text{Ir}(0)_n(\text{POct}_3)_{0.2n}$  nanoparticles, including their quantitative poisoning behavior,<sup>74,75</sup> there can be little doubt that minimally ligated, WLLL-derived nanoparticles such as  $\text{Ir}(0)_n(\text{POct}_3)_{0.2n}$  hold considerable

promise in catalysis and other applications. A wide range of other ligands, mixed ligand combinations, and other surface-directed chemistry should now be possible by the same route using the  $\text{Ir}(0)_n(\text{Cl}^- \text{H}^+)_b$  WLLL approach, as well as through further reactions of the isolable  $\text{Ir}(0)_n(\text{POct}_3)_{0.2n}$  nanoparticles as Scheme 2 begins to make apparent. Ligands of interest include those identified in prior, valuable studies by others.<sup>9,45,69–71</sup>

**$\gamma\text{-Al}_2\text{O}_3$ -Supported, Labile Ligand Nanoparticles-Derived  $\text{Ir}(0)_n(\gamma\text{-Al}_2\text{O}_3)(\text{Cl}^- \text{H}^+)$ .** The  $\text{Ir}(0)_n\text{H}^+\text{Cl}^-$  nanoparticle is also applicable to the synthesis of supported heterogeneous catalysts<sup>76–81</sup> (i.e., and as was hypothesized to be what was occurring when molecular sieves were added to  $\text{Ir}(0)_n\text{H}^+\text{Cl}^-$  nanoparticles previously<sup>59</sup>). The work that follows closely mirrors our previously published work,<sup>82–85</sup> but ties it into the  $\text{Ir}(0)_n\text{H}^+\text{Cl}^-$  nanoparticle WLLL and synthon concepts and, hence, is included in this report for the sake of completeness.

As before,<sup>82,83,85</sup> a supported version of the precatalyst,  $[\text{Ir}(1,5\text{-COD})\text{Cl}]/\gamma\text{-Al}_2\text{O}_3$ , was isolated first and then reduced under  $\text{H}_2$ , in acetone, and in the presence of cyclohexene (Scheme 5 (top)). A cyclohexene reporter reaction, shown in the bottom half of Scheme 5, allows one to monitor the

**Scheme 5. Stoichiometry, Synthesis Conditions, and Cyclohexene Hydrogenation Reaction of Interest for Ir(0)<sub>n</sub>/( $\gamma$ -Al<sub>2</sub>O<sub>3</sub>)(Cl<sup>-</sup>H<sup>+</sup>)-Supported Nanoparticle Heterogeneous Catalyst Formation<sup>82</sup>**



nanoparticle formation reaction.<sup>82,83,85</sup> The stoichiometry of the reaction was confirmed as before<sup>82</sup> by demonstrating (gas–liquid chromatography (GLC), and NMR) the evolution of  $1.0 \pm 0.1$  equiv of cyclooctane.<sup>82</sup>

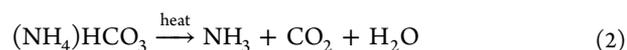
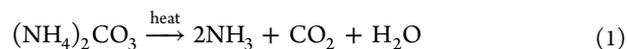
The observed sigmoidal kinetics along with the fit to the Finke–Watzky two-step mechanism of slow continuous nucleation ( $A \rightarrow B$ , rate constant  $k_1$ ), followed by fast autocatalytic surface growth ( $A + B \rightarrow 2B$ , rate constant  $k_2$ ) of this nanoparticle formation reaction,<sup>60</sup> implies that near-monodisperse ( $\leq \pm 15\%$  size dispersion<sup>14</sup>) nanoparticles should be formed.<sup>83,86</sup> Indeed, the resultant supported nanoparticles are  $2.9 \pm 0.4$  nm ( $\pm 14\%$ ) and are an active ( $24 \pm 5$  turnovers/s at  $22.0 \pm 0.1$  °C) and long-lived catalyst (360 000 total catalytic turnovers of cyclohexene hydrogenation).<sup>83</sup> These results both verify our prior work<sup>83,84</sup> and demonstrate that the Ir(0)<sub>n</sub>·H<sup>+</sup>Cl<sup>-</sup> WLL nanoparticle approach is of value in preparing supported-nanoparticle heterogeneous catalysts, specifically Ir(0)<sub>n</sub>/( $\gamma$ -Al<sub>2</sub>O<sub>3</sub>)(Cl<sup>-</sup>H<sup>+</sup>).

These catalysts contain only H<sup>+</sup>Cl<sup>-</sup>, cyclohexane, acetone solvent, and the support as possible ligands. The controlled reaction stoichiometry<sup>82</sup> and resultant product are therefore important aspects of the synthetic route to the present WLL nanoparticles. The WLL nanoparticle synthetic route and resultant supported nanoparticle have several advantages (i.e., compared to first forming the nanoparticles, depositing them on a support, and then trying—largely unsuccessfully<sup>16–25</sup>—to remove all of the stabilizing ligands<sup>86–88</sup>): (i) the WLL approach does not require the use of polymer or other, excessive or strong-binding ligands that can poison catalysis and block surface sites needed for other applications; (ii) the WLL approach eliminates separate nanoparticle isolation and deposition steps, and additionally (iii) the fit of the sigmoidal kinetics to the two-step mechanism imply that nine insights into the synthesis of nanoparticle catalysts<sup>86</sup> should also apply to the resultant products, including the following four chosen for illustration here: (a) the formation of near-monodisperse particles;<sup>82</sup> (b) the ability of the added ligands to attach to growing nanoparticle facets and induce shape control,<sup>82</sup> (c) size control over the resultant supported-nanoparticle heterogeneous catalyst;<sup>89</sup> and (iv) rational syntheses of all possible geometric isomers of, for example, bi- or multimetallic nanoparticles.<sup>82</sup> Overall, the results offer strong support for the efficacy of the WLL nanoparticle route to supported-nanoparticle heterogeneous catalysts.<sup>83,85</sup>

**Additional Possible Applications of WLL Nanoparticles.** A look back at Scheme 2 shows a couple of additional—among many other conceivable—uses of WLL nanoparticles. One is to make the nanoparticles in ionic liquids, well-known excellent stabilizers of nanoparticles, an application that already has good precedent,<sup>34,90–94</sup> particularly in Dupont and co-worker’s seminal studies starting with

[Ir(1,5-COD)Cl]<sub>2</sub> to form biphasic, ionic liquid-stabilized Ir(0)<sub>n</sub> nanoparticle alkene hydrogenation catalysts.<sup>91</sup>

Using volatile buffers as meta-stabilizing ligands is another, interesting, conceivable way to make a different version of WLL nanoparticles (Scheme 2) *vide supra*. The idea here is to use known volatile buffers, such as ammonium carbonate ((NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub>) and ammonium hydrogen carbonate ((NH<sub>4</sub>)-HCO<sub>3</sub>), as potential meta-stabilizers. If they could provide sufficient meta-stabilization, then these salts have the desirable, well-established property of being volatile (buffers) so that they could, then and in principle, conceivably be readily and completely removed under mild heat and vacuum conditions as shown in eq 1 (neat ammonium carbonate decomposing according to eq 1 at 60 °C and 1 atm, and in dodecane solution at 100 °C, for example<sup>95,96</sup>)



This idea intrigued us enough that we tested it experimentally, if just initially. The first problem we ran into is that neither ammonium carbonate nor ammonium hydrogen carbonate is soluble in acetone or propylene carbonate, the two organic solvents we have emphasized for our nanoparticle preparations. However, using (Bu<sub>3</sub>NH)<sub>2</sub>CO<sub>3</sub> in acetone generated in situ from [(1,5-COD)Ir(MeCN)<sub>2</sub>]<sub>2</sub>CO<sub>3</sub> with 1 equiv Bu<sub>3</sub>N (added as the base needed to scavenge H<sup>+</sup> generated in the H<sub>2</sub> reduction of the [(1,5-COD)Ir(I)<sup>+</sup>] moiety) followed by reduction under H<sub>2</sub> did yield a brown, nanoparticle-containing solution, which exhibited  $2.2 \pm 0.7$  nm particles by TEM. Unfortunately, once taken to vacuum to isolate them, the “Ir(0)<sub>n</sub>·(CO<sub>3</sub>)(Bu<sub>3</sub>NH)<sub>2</sub>” nanoparticles are not redispersible in acetone (see the SI for details), and hence apparently not sufficiently stabilized to be isolable. Accordingly, the “volatile buffer” approach is labeled in Scheme 2 as “undemonstrated”, but included here because of the interesting nature of the volatile buffer concept and the hope that suitable variations of it might work based on the creative ideas and efforts of others.

## CONCLUSIONS

In conclusion, the example of Ir(0)<sub>n</sub>·H<sup>+</sup>Cl<sup>-</sup> as a WLL, isolable, yet effectively coordinatively unsaturated nanoparticle system has been illustrated and expanded herein based on H<sub>2</sub> reduction of a [Ir(1,5-COD)Cl]<sub>2</sub> precatalyst in acetone. The use of the meta-stable Ir(0)<sub>n</sub>·H<sup>+</sup>Cl<sup>-</sup> as a valuable synthetic structural unit/building block was illustrated by the preparation of five specific nanoparticle products: Ir(0)<sub>n</sub>·(Cl<sup>-</sup>Bu<sub>3</sub>NH<sup>+</sup>)<sub>a</sub>, Ir(0)<sub>n</sub>·(Cl<sup>-</sup>Dodec<sub>3</sub>NH<sup>+</sup>)<sub>a</sub>, Ir(0)<sub>n</sub>·(POct<sub>3</sub>)<sub>a</sub>(Cl<sup>-</sup>H<sup>+</sup>)<sub>b</sub>, Ir(0)<sub>n</sub>·(POct<sub>3</sub>)<sub>a</sub>, and the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>-supported heterogeneous catalyst, Ir(0)<sub>n</sub>·( $\gamma$ -Al<sub>2</sub>O<sub>3</sub>)<sub>a</sub>(Cl<sup>-</sup>H<sup>+</sup>)<sub>b</sub>. In the case of the Ir(0)<sub>n</sub>·(Cl<sup>-</sup>Bu<sub>3</sub>NH<sup>+</sup>)<sub>a</sub> nanoparticles, it was shown that HCl could be quantitatively ( $\geq 98\%$ ) removed by mild heating, opening the door for removal of the volatile HCl in cases where doing so is desired. Removing HCl from Ir(0)<sub>n</sub>·(POct<sub>3</sub>)<sub>0.2</sub>(Cl<sup>-</sup>H<sup>+</sup>)<sub>b</sub> in vacuum at 30 °C yields isolable and redispersible Ir(0)<sub>n</sub>·(POct<sub>3</sub>)<sub>0.2</sub> nanoparticles  $\geq 99\%$  free of HCl, nanoparticles that can be weighed out as a solid for any desired application, and nanoparticles that retain their high catalytic activity post redispersion in acetone.

The case of the POct<sub>3</sub>-stabilized nanoparticles, Ir(0)<sub>n</sub>·(POct<sub>3</sub>)<sub>0.2</sub>, is especially significant in that just 0.2 equiv of POct<sub>3</sub> was demonstrated to provide well-formed, reasonably

well-stabilized, size-controlled  $\text{Ir}(0)_{\sim 150}$  nanoparticles—thereby opening up in-progress quantitative kinetic, mechanistic, SAXS, and other studies of size control as a function of precisely known amounts of added ligand, L, which start from  $\ll 1$  equiv of L per metal present in  $\text{Ir}(0)_n \cdot (\text{POct}_3)_{0.2}$ .

Presented in Scheme 2 are additional possibilities for exploiting the WLLL nanoparticle concept, for example, the use of other, readily removable ligands such as volatile buffers. The ready commercial availability of labile ligand organometallic precursors/precatalysts analogous to  $[(1,5\text{-COD})\text{IrCl}]_2$  such as  $[(1,5\text{-COD})\text{RhCl}]_2$ ,  $(1,5\text{-COD})\text{PtCl}_2$ ,  $\text{Ru}(\text{COD})(\text{COT})$ , as well as other precursors that one can imagine to labile ligand nanoparticles fuels our hope that others will add to and expand the examples and applications of WLLL nanoparticles in their own research.

## EXPERIMENTAL SECTION

**Materials.** All commercially obtained reagents were used as received unless otherwise noted. All solvents were stored in a  $\leq 1$  ppm  $\text{O}_2$  drybox prior to use. Acetone packed under nitrogen was purchased from Burdick & Jackson (water content  $< 0.5\%$ ). Cyclohexene (Aldrich, 99%) was freshly distilled over sodium metal under argon and stored in a predried glass bottle.  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  (STREM), tris(dodecyl)amine (Aldrich, 97%), trioctylphosphine (Aldrich, 97%), and tributylamine (Aldrich,  $\geq 99.5\%$ ) were stored in a drybox. Solutions (1.0 M) of proton sponge (Aldrich) in acetone were freshly made. Acidic  $\gamma\text{-Al}_2\text{O}_3$  (Aldrich) with a surface area of  $155 \text{ m}^2/\text{g}$  was dried at  $160 \text{ }^\circ\text{C}$  for 24 h and stored in the drybox prior to use.  $\text{CD}_2\text{Cl}_2$  (Cambridge Isotope Laboratories) from 1 mL glass ampoules were transferred into the drybox for NMR sample preparation.  $\text{H}_2$  gas was purchased from General Air in  $>99.5\%$  purity and passed through  $\text{O}_2$  and  $\text{H}_2\text{O}$  scavenging traps (Trigon Technologies) before use to pressurize Fisher-Porter (FP) bottle reactors (vide infra).

**Analytical Instrumentation and Procedures.** Unless otherwise reported, all reaction solutions were prepared under oxygen and moisture-free conditions in a Vacuum Atmospheres nitrogen-filled drybox. The  $\text{O}_2$  level ( $\leq 1$  ppm  $\text{O}_2$ ) was continuously monitored by a Vacuum Atmospheres  $\text{O}_2$  sensor. Gas-liquid chromatography (GLC) was performed using a Hewlett-Packard 5890 Series II GC with a flame ionization detector equipped with a 30 m (0.25 mm i.d., 25  $\mu\text{m}$  film) Supelco SPB-1 column coupled with a Hewlett-Packard 3395 integrator. The GLC parameters are: initial temperature,  $50 \text{ }^\circ\text{C}$ ; initial time, 3 min; ramp,  $10 \text{ }^\circ\text{C}/\text{min}$ ; final temperature,  $160 \text{ }^\circ\text{C}$ ; final time, 16 min; injector port temperature,  $180 \text{ }^\circ\text{C}$ ; detector temperature,  $200 \text{ }^\circ\text{C}$ ; and injection volume, 2 or 4  $\mu\text{L}$ . High-resolution  $^1\text{H}$  (300.115 MHz) and  $^{13}\text{C}$  (75.472 MHz) NMR spectra were taken on a Varian INOVA-300 spectrometer. Thermogravimetric analysis (TGA) was carried out in a TA Instruments TA 2950 thermogravimetric analyzer (with integrated Balzers mass spectrometer) using Pt pans, in a He purged atmosphere. The ramping rate used was  $2 \text{ }^\circ\text{C}/\text{min}$  until the appropriate temperature was reached. TEM analysis was done using a Philips CM-12 TEM with a 70  $\mu\text{m}$  lens operating at 100 kV and with a 2.0  $\text{Å}$  point-to-point resolution, and a JEOL JEM-2100F transmission electron microscope operating at 200 kV was used to take bright-field STEM images of iridium(0) nanoparticles deposited on an silicon nitride grid (Ted Pella, Inc.). TEM images were analyzed by using Public-Domain Image-Processing Program.<sup>97</sup> Typically, TEM pictures

of each sample were taken at three different magnifications (100, 200, and 430 K) to obtain information about the sample.

**Hydrogenation Apparatus and Data Handling.** Hydrogenation experiments were carried out in a custom-built, previously described<sup>73</sup> apparatus to continuously monitor hydrogen pressure loss. Briefly, the apparatus consists of a Fisher-Porter (FP) bottle modified with Swagelok TFE-sealed quick-connects to both a  $\text{H}_2$  line and an Omega PX621 pressure transducer. The pressure transducer is interfaced to a PC via an Omega D1131 5 V A/D converter with an RS-232 connection. Pressure uptake data were collected using LabView 7.1 and analyzed using Origin 7.0 when the data could be fit to the known two-step autocatalytic mechanism.<sup>60</sup> The hydrogen uptake curves were converted to cyclohexene consumption curves before analyzing via Origin 7.0, which is done by using the known 1:1  $\text{H}_2$  to cyclohexene stoichiometry and the previously established cyclohexene reporter reaction kinetic method.<sup>60</sup>

**Preparation of  $\text{Ir}(0)_n \cdot \text{H}^+\text{Cl}^-$  Nanoparticles for Acetone Hydrogenation.** As previously described and reproduced as a control experiment,<sup>59</sup> in a 2 dram glass vial, 1.2 mg (3.6  $\mu\text{mol}$  of Ir) of the precatalyst  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  was weighed and dissolved in 0.5 mL (6.7 mmol) of acetone (added with a 1.0 mL gastight syringe), to yield a clear, yellow solution. The solution was then transferred via a disposable polyethylene pipet into a new  $22 \times 175 \text{ mm}^2$  Pyrex culture tube containing a new  $5/16 \text{ in.} \times 5/8 \text{ in.}$  Teflon-coated stir bar. The culture tube was then sealed inside the FP bottle, brought outside the drybox, placed in a constant-temperature water-circulating bath at  $22.0 \pm 0.1 \text{ }^\circ\text{C}$ , and attached via Swagelok TFE-sealed quick-connects to the hydrogenation line described in the above section. Stirring was started ( $>600 \text{ rpm}$ ; this stirring rate is important to avoid  $\text{H}_2$  gas-to-solution mass-transfer limitations), and the FP bottle was then purged 15 times with hydrogen (15 s per purge), stirred vigorously for an additional 30 s, and then  $t = 0$  was noted.

**Preparation of  $\text{Ir}(0)_n \cdot \text{Bu}_3\text{NH}^+\text{Cl}^-$  Stabilized Nanoparticles.** In the drybox, 1.8  $\mu\text{mol}$  (3.6  $\mu\text{mol}$  in Ir)  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  was weighed into a 2 dram predried glass vial. Subsequently, 2.5 mL of acetone and 0.5 mL of cyclohexene were added via gastight syringes to the 2 dram vial. Next, 3.6  $\mu\text{mol}$  tributylamine was added to the vial, and the resulting solution was mixed with a disposable polyethylene pipette and transferred into a new borosilicate culture tube ( $22 \times 175 \text{ mm}^2$ ) with a new  $5/8 \text{ in.} \times 5/16 \text{ in.}$  Teflon-coated octagon-shaped stir bar. A standard conditions hydrogenation was performed following the previously developed procedure.<sup>73</sup>

**Preparation of  $\text{Ir}(0)_n \cdot \text{POct}_3$ -Stabilized Nanoparticles.** Preparation of trioctylphosphine stock solution: In the drybox, 1.0 mmol  $\text{POct}_3$  was transferred via a 1 mL gastight syringe from the bottle (Aldrich, 97%) into a septum-sealed, 20 mL bottle by weighing the amount of transferred liquid. Then, 9.6 mL of cyclohexane was added to the bottle. The total volume of solution was 10.0 mL, and the concentration of  $\text{POct}_3$  was 100 mM. A 100  $\mu\text{L}$  aliquot of this solution was transferred into a 5.0 mL volumetric flask, and the volume was completed to 5.0 mL by adding cyclohexane. The  $\text{POct}_3$  concentration of this solution was 2.0  $\mu\text{mol}/\text{mL}$ . A preselected aliquot of this solution, to achieve the desired concentrations noted in experiments in the main text, was then added to the precatalyst solution.

In a 2 dram glass vial, 1.2 mg (3.6  $\mu\text{mol}$  of Ir) of the precatalyst  $[\text{Ir}(1,5\text{-COD})\text{Cl}]_2$  was weighed and dissolved in

2.14 mL of acetone to yield a clear, yellow solution. The solution was then transferred via a disposable polyethylene pipet into a new 22 × 175 mm<sup>2</sup> Pyrex culture tube containing a new 5/16 in. × 5/8 in. Teflon-coated stir bar. To this solution, a 360 μL aliquot of the trioctylphosphine solution (360 μL × 2.0 μmol/mL = 0.72 μmol POct<sub>3</sub>) and 0.5 mL of cyclohexene were added. A standard conditions hydrogenation was performed following the previously developed procedure.<sup>73</sup>

After the first run of hydrogenation, the FP bottle was taken into the drybox. The solution in the culture tube was connected to vacuum and brought to dryness for 3 h (10<sup>-1</sup> Torr, 25 °C). The residue in the culture tube was redispersed in 2.5 mL of acetone. After addition of 0.5 mL of cyclohexene, the culture tube was then sealed inside the FP bottle, brought outside the drybox, placed in a constant-temperature water-circulating bath at 22.0 ± 0.1 °C, and attached via Swagelok TFE-sealed quick-connects to the hydrogenation line. A standard conditions hydrogenation was then performed following the previously developed procedure.<sup>73</sup>

**Catalyst Lifetime Experiments from [Ir(1,5-COD)Cl]<sub>2</sub> with Added Bu<sub>3</sub>N.** The catalyst lifetime experiment was performed identically to those previously published.<sup>59</sup> In the drybox, 0.72 μmol [Ir(COD)Cl]<sub>2</sub> and 0.72 μmol Bu<sub>3</sub>N were dissolved in 4.5 mL of acetone added via a 10 mL gastight syringe. The resulting solution was mixed using a disposable polyethylene pipette and transferred into a new borosilicate culture tube (22 × 175 mm<sup>2</sup>) with a new 5/8 in. × 5/16 in. Teflon-coated octagon-shaped stir bar. Next, 4.5 mL (44 mmol, corresponding to a maximum of 61 000 turnovers) of cyclohexene was added to the culture tube and then the FP bottle was sealed and brought out of the drybox. The FP reactor was purged and set to 40 psig, as described above.

The reaction was monitored by periodically withdrawing aliquots of the reaction solution for <sup>1</sup>H NMR spectroscopy. This monitoring was accomplished by sealing the FP bottle, disconnecting it from the hydrogenation line and then transferring the vessel back into the drybox. Aliquots were removed inside the drybox by using a 9 in. glass Pasteur pipette inserted into the reaction solution and drawing out 0.05 mL of aliquots. The aliquot was then added to 1 g of CDCl<sub>2</sub> in an individual glass ampoule and mixed using a Pasteur pipette, which was then transferred to an NMR tube. The FP bottle was then resealed, taken out of the drybox, reconnected to the H<sub>2</sub> line, and the above-noted purge cycle with H<sub>2</sub> to restart the hydrogenation reaction was repeated. The NMR tube containing the reaction aliquot was sealed and brought out of the drybox, and a <sup>1</sup>H NMR spectrum was obtained.

**Preparation of Ir(0)<sub>n</sub>/γ-Al<sub>2</sub>O<sub>3</sub>-Stabilized Nanoparticles.** The precatalyst solutions were prepared in the drybox using preselected [Ir(1,5-COD)Cl]/support weight-to-weight ratios following the procedure described elsewhere.<sup>82</sup> Each individual sample was then transferred via a disposable polyethylene pipette into the new borosilicate culture tube (22 × 175 mm<sup>2</sup>) containing a new 5/8 in. × 5/16 in. Teflon-coated octagon-shaped stir bar. A standard conditions hydrogenation was performed following the previously developed procedure.<sup>73</sup>

**Preparation of TEM Grids.** Following the hydrogenation of cyclohexene (and acetone) and the formation of nanoparticles, the FP bottle was sealed, disconnected from the H<sub>2</sub> line, and transferred into the drybox. The reaction solution was quantitatively transferred with a disposable polyethylene pipette into a clean, 5 mL screw-capped glass vial. The

solution was dried under vacuum of <10<sup>-1</sup> Torr at 30 °C for 3 h and then the glass vial was sealed and brought out of the drybox. The dry nanoparticle samples were sent as solids (in screw-capped glass vials) to Clemson University for TEM investigation. There, 1 mL of acetonitrile was added just before the TEM was obtained. A drop of this solution was then redispersed on a chloroform-cleaned, carbon-coated Cu TEM grid. Ir(0)<sub>n</sub>/γ-Al<sub>2</sub>O<sub>3</sub> TEM samples were prepared by dipping a TEM grid into the resultant nanoparticle solution for 5 s.

The solutions used for the preparation of grids for bright-field STEM images were exactly the same ones prepared in the respective sections above. At the end of complete hydrogenation of cyclohexene (and acetone), the FP bottle was detached from the hydrogenation line via its quick-connects, brought back into the drybox, and its acetone solution was quantitatively transferred with a disposable polyethylene pipette into a clean, 2 dram glass vial. A 0.2 mL aliquot of the solution was added into 1 mL 2-butanone in the 2 dram vial for dilution, 0.1 μL of the diluted solution was dropped via a micropipette on a silicon nitride grid, and the excess liquid was removed by quickly wicking away from the lower edge of grid. The grids were left in the drybox for drying for a minimum of 2 h prior to start with the electron microscopy analysis.

**Thermogravimetric Analysis Sample Preparation for [(1,5-COD)IrCl]<sub>2</sub> with Bu<sub>3</sub>N.** Two scaled up hydrogenations containing 3.6 μmol [(1,5-COD)IrCl]<sub>2</sub> and 7.2 μmol Bu<sub>3</sub>N, 2.5 mL of acetone, and 0.5 mL of cyclohexene were performed. The nanoparticle solutions were transferred into the drybox and combined. The volatiles (acetone and cyclohexane) were gently removed under vacuum of <10<sup>-1</sup> Torr at 30 °C in an effort to minimize the possible loss of Bu<sub>3</sub>N and HCl in this necessary step. The black residue was then transferred into an aluminum TGA capsule and sealed in the drybox by mechanical press. Immediately prior to TGA analysis, a hole was placed in the capsule and the sample pan was placed in the TGA for analysis.

## ■ ASSOCIATED CONTENT

### 📄 Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acsomega.8b01569.

Literature reports of naked nanoparticles; plot of cyclohexene loss versus time for the hydrogenation of 1.65 M cyclohexene starting with 3.6 μmol [(1,5-COD)IrCl]<sub>2</sub> and 7.2 μmol Bu<sub>3</sub>N; plot of cyclohexene loss vs time for the second run of hydrogenation of 1.65 M cyclohexene by using isolated Ir(0) nanoparticles and TEM imaging of sample harvested after reaction; evolution of the total turnovers (TTOs) of cyclohexene hydrogenation and TEM image of the sample harvested after the catalytic lifetime measurement; plot of cyclohexene loss vs time in the second run of hydrogenation of 1.65 M cyclohexene using the Ir(0) nanoparticles formed initially, and in a first run of cyclohexene hydrogenation starting with 0.6 mM [(1,5-COD)IrCl]<sub>2</sub> and 1.2 mM dodecyl<sub>3</sub>N; attempted formation of volatile buffer-stabilized Ir(0) nanoparticles using alkylammonium carbonate; attempted formation of tetrabutylammonium carbonate-stabilized Ir(0) nanoparticles; attempted formation of tributylammonium

carbonate-stabilized Ir(0) nanoparticles in acetone; plot of cyclohexene loss versus time curve for the hydrogenation of 1.65 M cyclohexene starting with 0.6 mM [(1,5-COD)Ir]<sub>2</sub>CO<sub>3</sub> and 0.6 mM [Bu<sub>3</sub>NH]<sub>2</sub>CO<sub>3</sub>; attempted formation of tributylammonium carbonate-stabilized Ir(0) nanoparticles using [(1,5-COD)Ir(CH<sub>3</sub>CN)<sub>2</sub>]<sub>2</sub>CO<sub>3</sub> as precursor in acetone; plot of cyclohexene loss versus time in the hydrogenation of 1.65 M cyclohexene starting with 0.6 mM [(1,5-COD)Ir]<sub>2</sub>CO<sub>3</sub> and 1.2 mM proton sponge and TEM image of the sample harvested after reaction; and TGA of the tributylammonium carbonate-stabilized Ir(0) nanoparticles obtained from the hydrogenation of [(1,5-COD)Ir(CH<sub>3</sub>CN)<sub>2</sub>]<sub>2</sub>CO<sub>3</sub> and 1.2 mM Bu<sub>3</sub>N (PDF)

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### Notes

The authors declare no competing financial interest.

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## ADDITIONAL NOTE

<sup>a</sup>The average size of the iridium(0) nanoparticles was estimated on the basis of an assumed face-centered cubic structure for iridium:  $n = (N_0 \rho (4/3) \pi (D/2)^3) / W$ ,<sup>73</sup> where  $n$  is the number of Ir atoms,  $N_0 = 6.022 \times 10^{23} \text{ mol}^{-1}$ ,  $\rho$  is the room-temperature density of iridium (22.5 g/cm<sup>3</sup>),  $D$  is the diameter of iridium nanoparticles, and  $W$  is the atomic weight of iridium (192.22 g/mol).<sup>72</sup> This calculation yields Ir<sub>~150</sub> for an average diameter of ~1.5 nm.

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